

Investigation of diesel particle deposition in tubes

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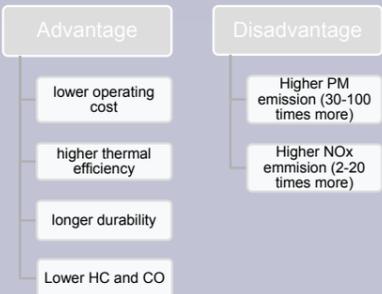
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Abstract

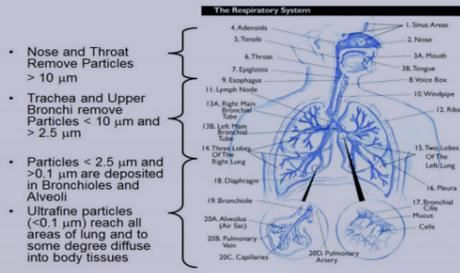
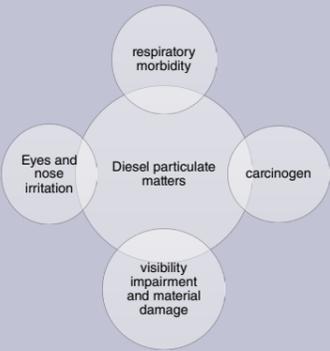
- Plasma treatment reactors have recently been developed for the elimination of diesel particulate matter regarding the reduction of both particle mass and number.
- The role of the plasma itself is obscured by the phenomenon of particle deposition on the surface of the reactor.
- Lagrangian particle tracking provides an effective method for simulating deposition of nano-particles
- The deposition of nano-particles in annular tubes under laminar condition is studied in this study.
- The role of particle diameter, reactor length and flow rates are examined.

Motivation

Advantage and disadvantage of diesel engines compared to gasoline engine [1]:

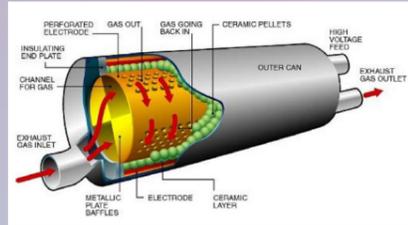


Negative effects of diesel particulate matters [1]:

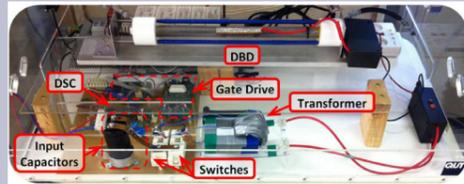


Experimental setup

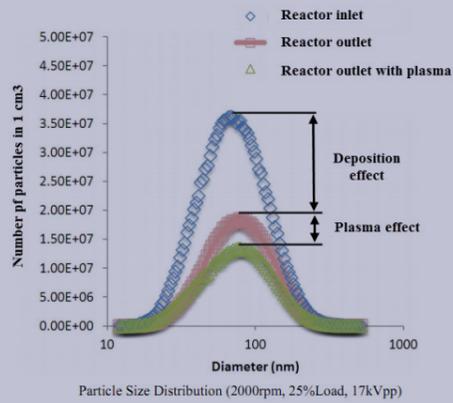
Non thermal plasma as a promising new technology for NOx and PM removal [2]:



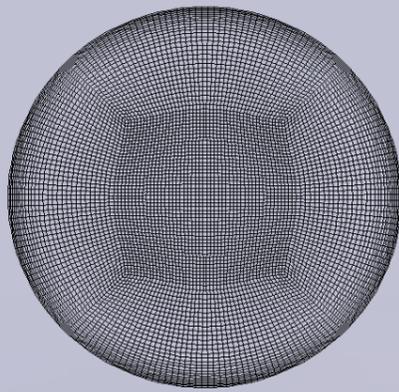
Non thermal plasma for PM mass and number removal [3]:



Deposition effect VS. Plasma effect [3]:



Mesh structure at cross section:



Numerical procedure

1. CFD solution of Navier Stokes Equations for the flow field

$$\rho \frac{DV}{Dt} = F - \nabla P + \mu \nabla^2 V$$

2. Particle equation of motion to model deposition and dispersion of particles

$$\frac{du_i^p}{dt} = -\frac{18\mu}{d_p^2 \rho_p C_c} (u_i^g - u_i^p) + F_{Brownian}$$

u_i^g and u_i^p : Components of the particle and local fluid velocity
 μ : Fluid viscosity
 ρ_p : Particle density
 C_c : Cunningham correction factor to Stokes' drag law

$$F_{Brownian} = \frac{\zeta}{m_d} \sqrt{\frac{1}{\tilde{D}} \frac{2k_B T^2}{\Delta t}}$$

Diffusion coefficient

$$\tilde{D} = \frac{k_B T C_c}{3\pi\mu d_p}$$

d_p : Particle diameter (m)

Boundary condition

Flow

- Parabolic velocity profile at the inlet
- Outflow at the outlet
- No slip condition at the wall

Particle

- Injection of 70000 particles at 1cm from the inlet and 0.1 mm away from the wall
- Escape condition at the outlet
- Trap condition at the wall

Ingham equation

$$DE = 1 - \left(0.819e^{-14.63\Delta} + 0.0976e^{-89.22\Delta} + 0.0325e^{-228\Delta} + 0.0509e^{-125.9\Delta^{2/3}} \right)$$

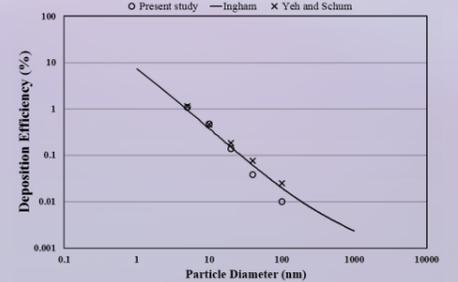
Δ is the dimensionless diffusion parameter

$$\Delta = \frac{\tilde{D} L_{pipe}}{4U_{in} R^2}$$

L_{pipe} : Pipe length
 R : Pipe radius
 U_{in} : Inlet velocity of the pipe

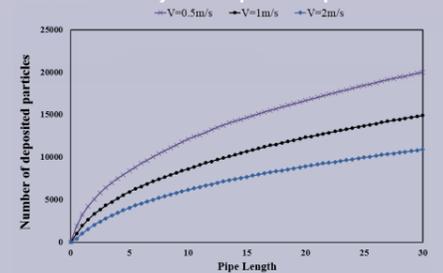
Results

1. Validation

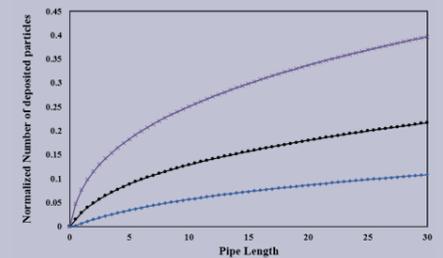


The variation of nano particle deposition efficiency as a function of particle diameter at the inlet velocity of 1 m/s.

2. Parametric study of nano-particle deposition



Effect of inlet velocity on the deposition of 5nm particles through the pipe length



Effect of pipe diameter on the deposition of 5nm particles through the pipe length

Emission standards over time for diesel cars in Japan, EU, and the USA [6]:

Country	Standard	Date	CO	HC	HC+NOx	NOx	PM	PN
			g/km					#/km
Emission Standards for Diesel Passenger Cars								
Japan	Vehicle weight							
	< 1250 kg	2002	0.63	0.12		0.28	0.052	
		2005	0.63	0.024		0.14	0.013	
		2009	0.63	0.024		0.08	0.005	
	> 1250 kg	2002	0.63	0.12		0.3	0.056	
		2005	0.63	0.024		0.15	0.014	
2009		0.63	0.024		0.08	0.005		
Emission Standards for Diesel Passenger Cars								
EU	Euro 4	2005.01	0.5		0.3	0.25	0.025	
	Euro 5a	2009.09	0.5		0.23	0.18	0.005	
	Euro 5b	2011.09	0.5		0.23	0.18	0.005	6E+11
	Euro 6	2014.09	0.5		0.17	0.08	0.005	6E+11
LEV II Emission Standards for Passenger Cars and LDVs < 8500 lbs; 50,000 miles/5 years								
US California			CO	HCHO	NMOG	NOx	PM	
			g/mile					
	LEV	2004-2010	3.4	0.015	0.075	0.05		
	ULEV		1.7	0.008	0.04	0.05		
SULEV								

Note: PN - Particle Number, NMOG - non-methane organic gases, HCHO - formaldehyde, LEV-Low Emission Vehicles, ULEV-Ultra Low Emission Vehicles, SULEV-Super Ultra Low Emission Vehicles

Emissions Requirements for Diesel Heavy Duty Vehicles in Australia [7]:

Country	Standard	Date	CO	HC	HC+NOx	NOx	PM	PN
			g/kWh					
AU	ADR80/02 (Stationary Cycle)	2007-2008	1.5	0.46	-	3.5	0.02	-
	ADR80/02 (Transient Cycle)		4.0	0.55	-	3.5	0.03	-
	ADR80/02 (Stationary Cycle)	2010-2011	1.5	0.46	-	2.0	0.02	-
	ADR80/02 (Transient Cycle)		4.0	0.55	-	2.0	0.03	-

Conclusion

- The advantage of lagrangian particle tracking method due to considering particle inertia than the Eulerian method
- Increasing particle deposition efficiency by decreasing inlet velocity and pipe diameter
- Decreasing the ratio of number of deposited particles by increasing the length of the pipe
- For nano particles with the diameter more than 40nm, the calculated DE is less than Eulerian method due to statistical error or the inertia effect.

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