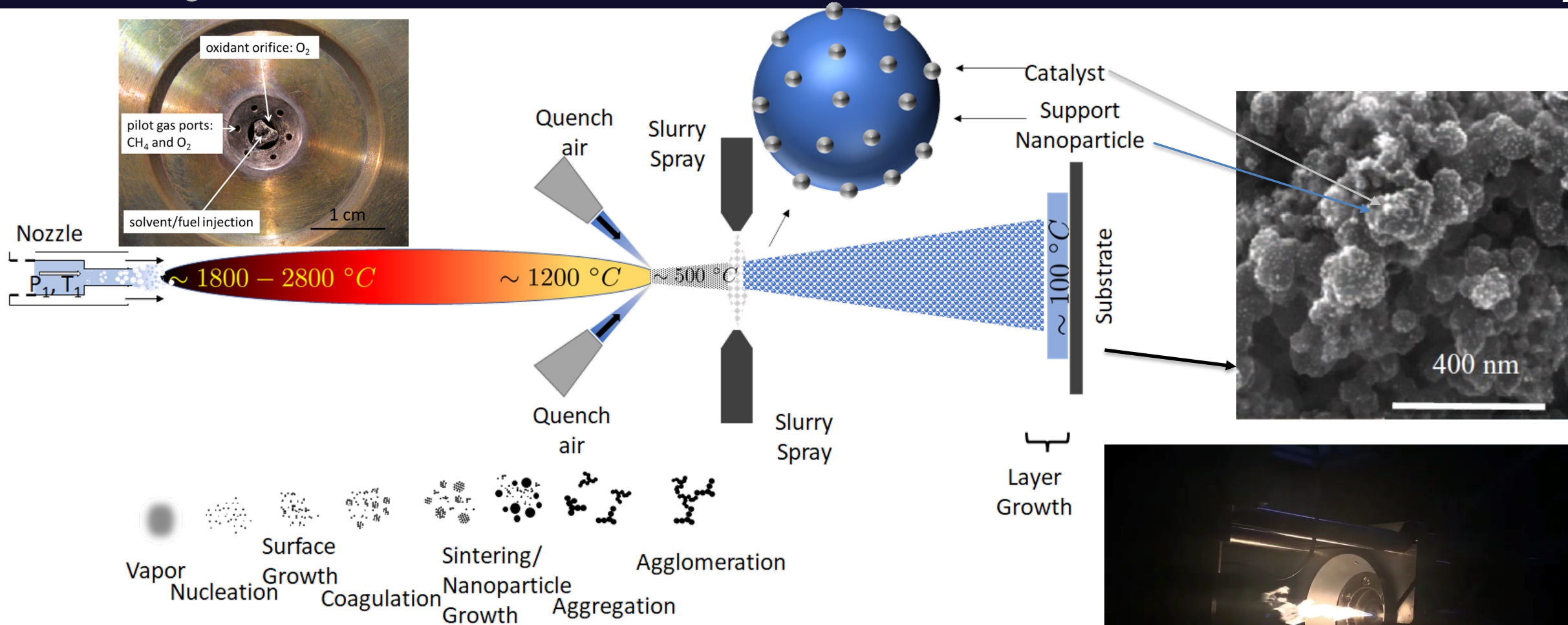


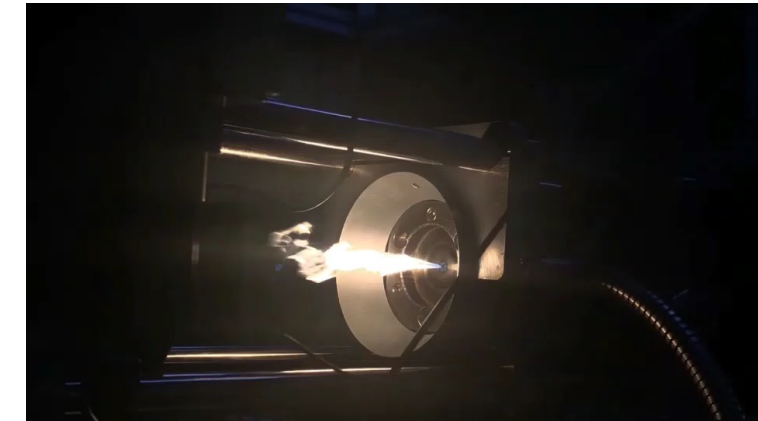
IN-SITU CHARACTERIZATION OF CATALYST NANOPARTICLES FROM REACTIVE SPRAY DEPOSITION TECHNOLOGY (RSDT)

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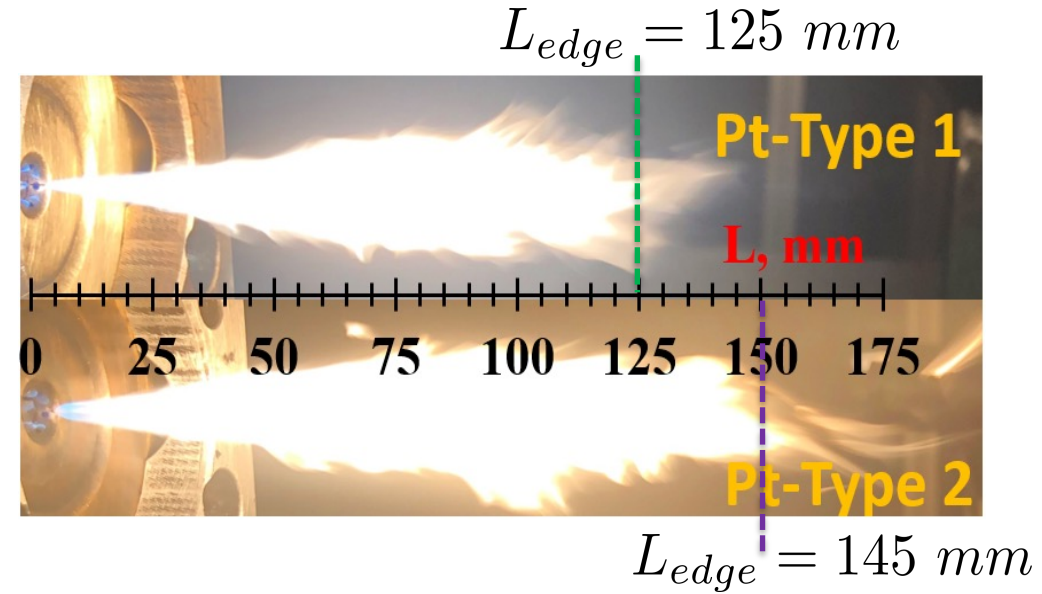


One-step flame-based process which is used in fuel cell, electrolyzer, and battery catalyst layer manufacturing

- ❑ Synthesized nanoparticles < 10nm
- ❑ Process optimization could be accelerated by in-situ measurements (e.g. particle size distribution, number concentration)



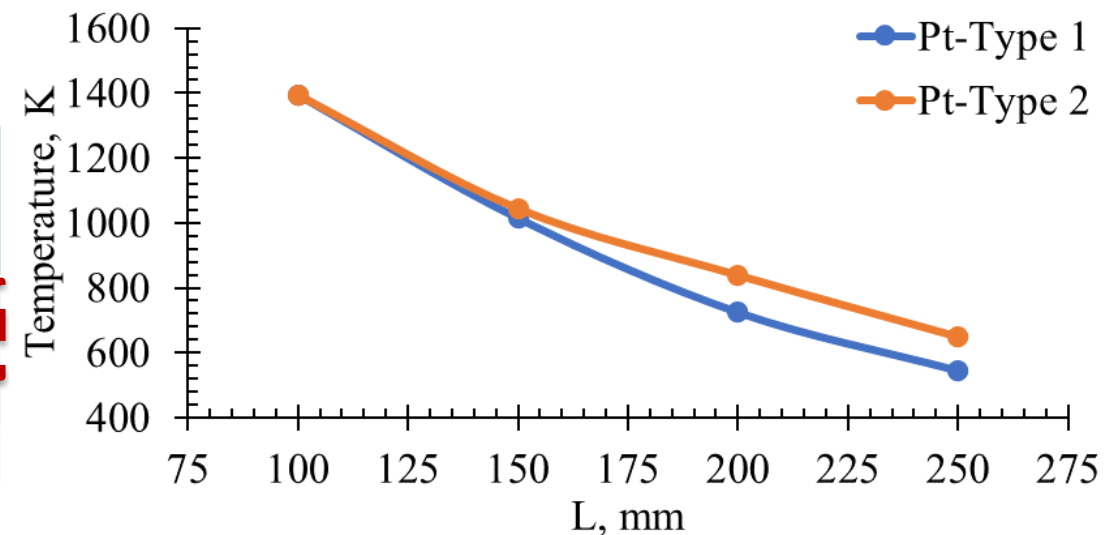
- ❑ Two pairs of flames with different liquid fuel flowrates
- ❑ The two flames of the pairs differ only on the presence and the absence of the precursor (PtAcAc) in the solution
- ❑ The average image of the flame is utilized to measure the flame length



Solvents in liquid fuel: acetone, xylene, liquid propane

Precursor: Platinum Acetylacetonate (PtAcAc)

Flame name	Liquid fuel mixture (mL/min)	O ₂ (SLPM)	Pilot CH ₄ flow rate (SLPM)	Pilot O ₂ flow rate (SLPM)	PtAcAc in liquid fuel
Pt-Type 1	4	7.3	0.55	0.55	10 mM
Pt-Blank 1	4	7.3	0.55	0.55	-
Pt-Type 2	7	11	0.75	0.75	10mM
Pt-Blank 2	7	11	0.75	0.75	-

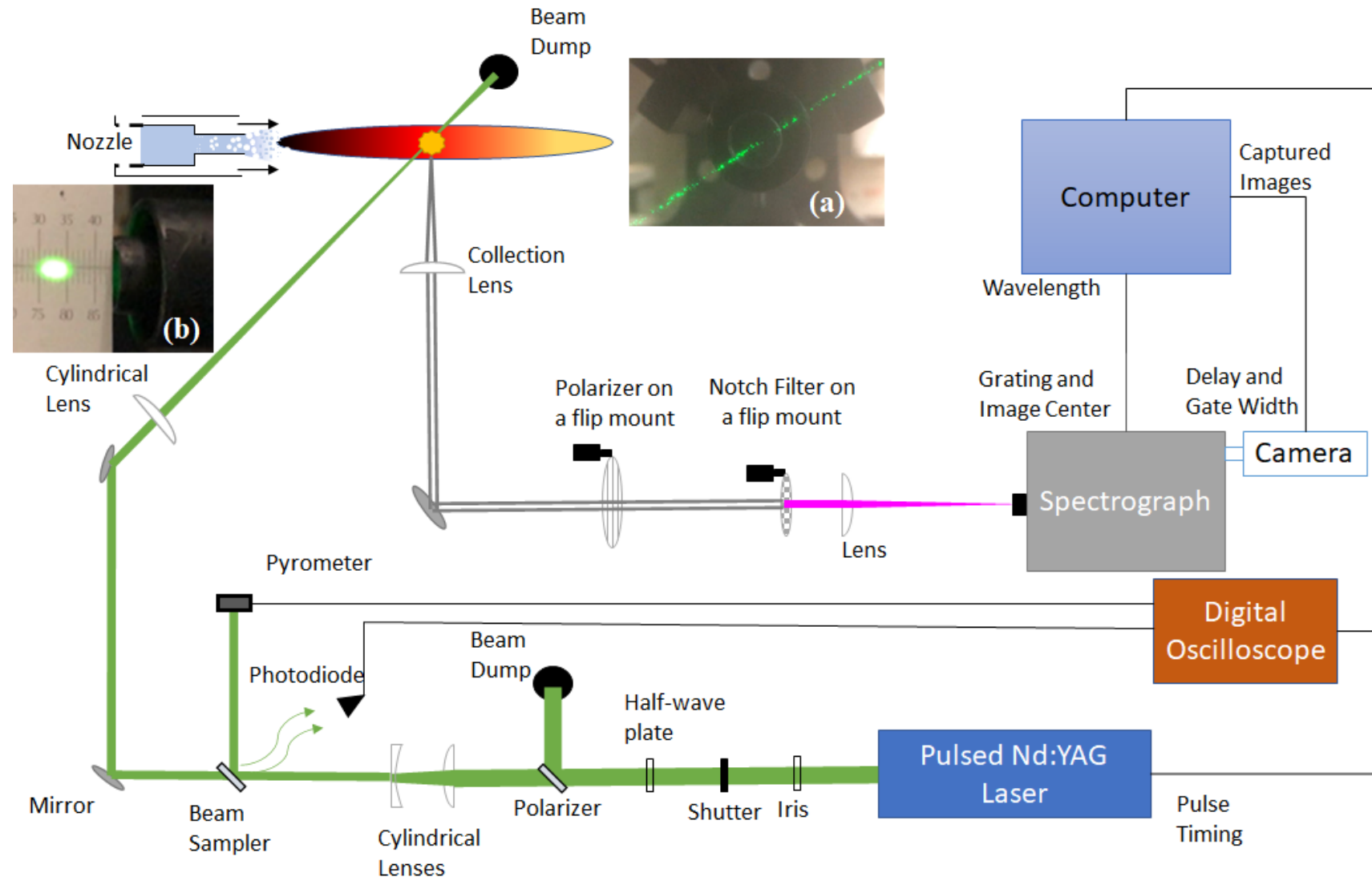


❑ Light Scattering (LS)

- Gate time 20 ns
- Polarizer installed
- No Notch filter

❑ Laser Induced Incandescence (LII)

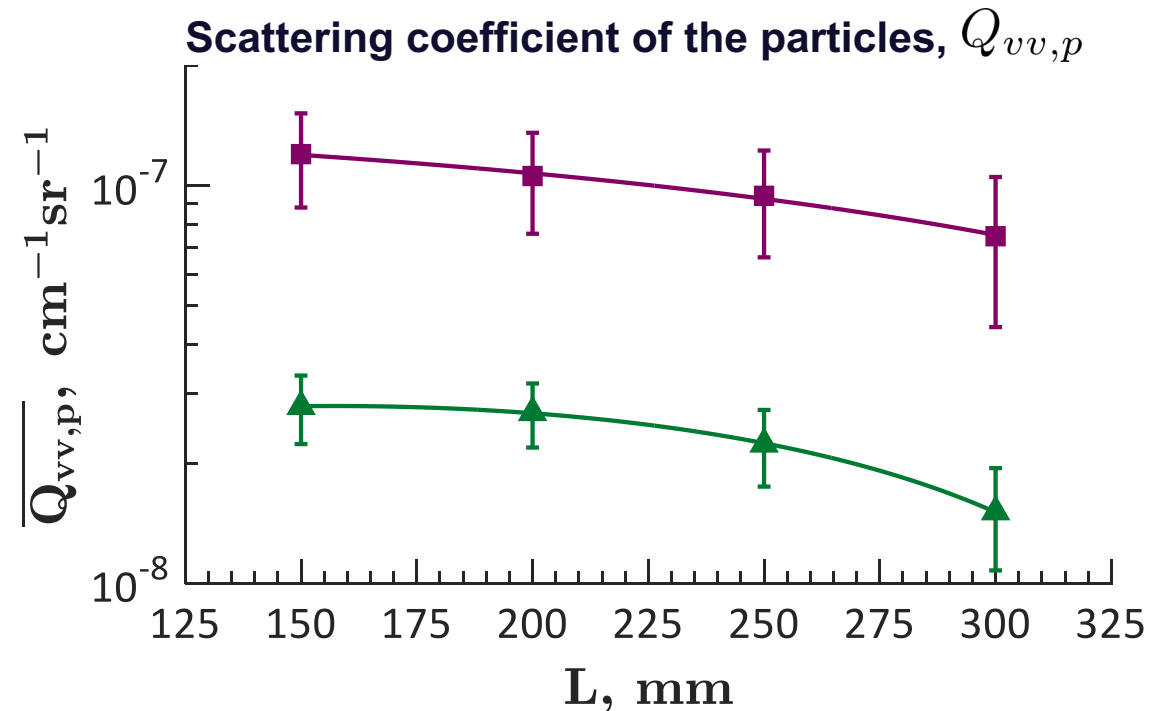
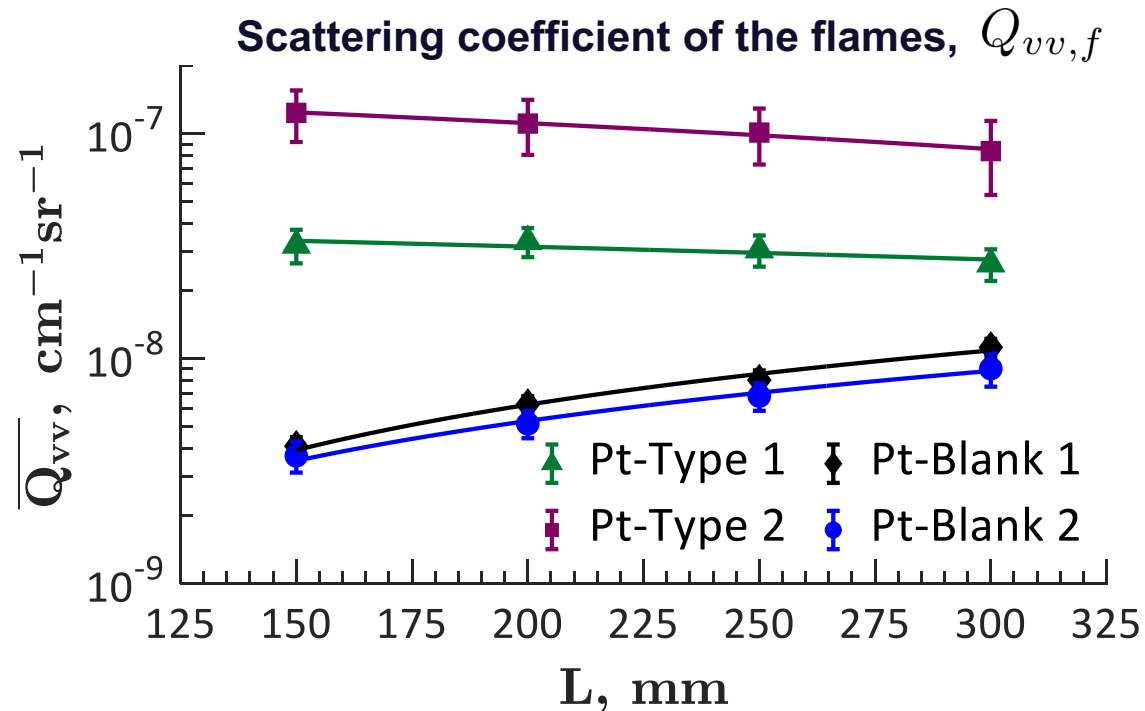
- Gate time
 - 150 ns
 - 250 ns
 - 350 ns
- No polarizer
- Notch filter installed



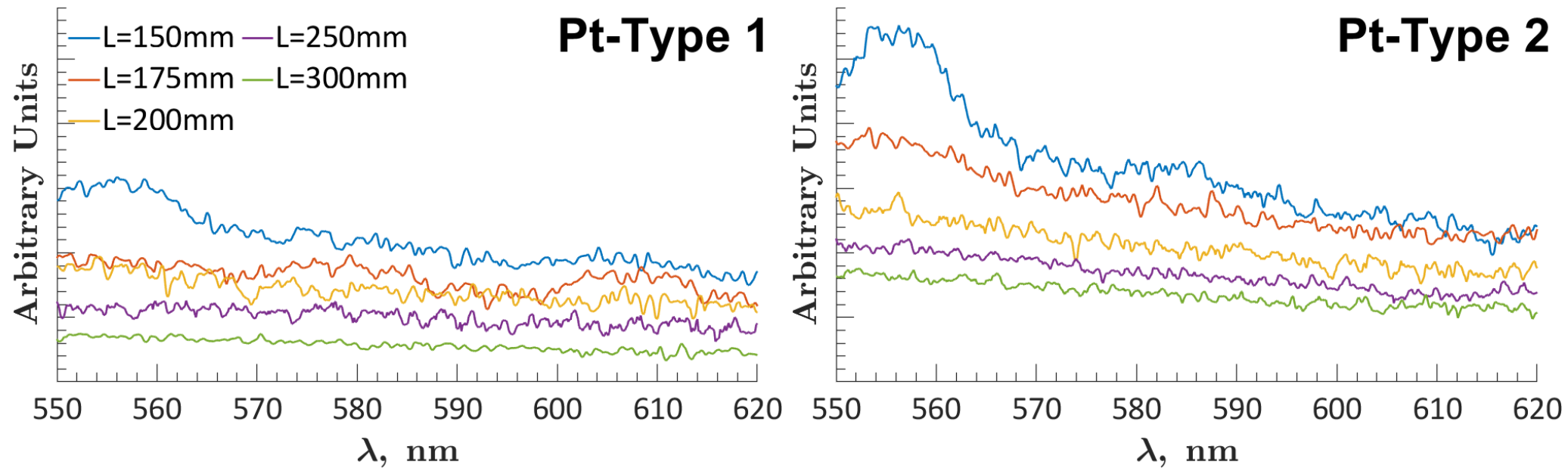
$Q_{vv,Pt}$:scattering coefficient of the Pt flame
 $Q_{vv,Blank}$:scattering coefficient of the Blank flame

$$Q_{vv,p} = Q_{vv,Pt} - Q_{vv,Blank}$$

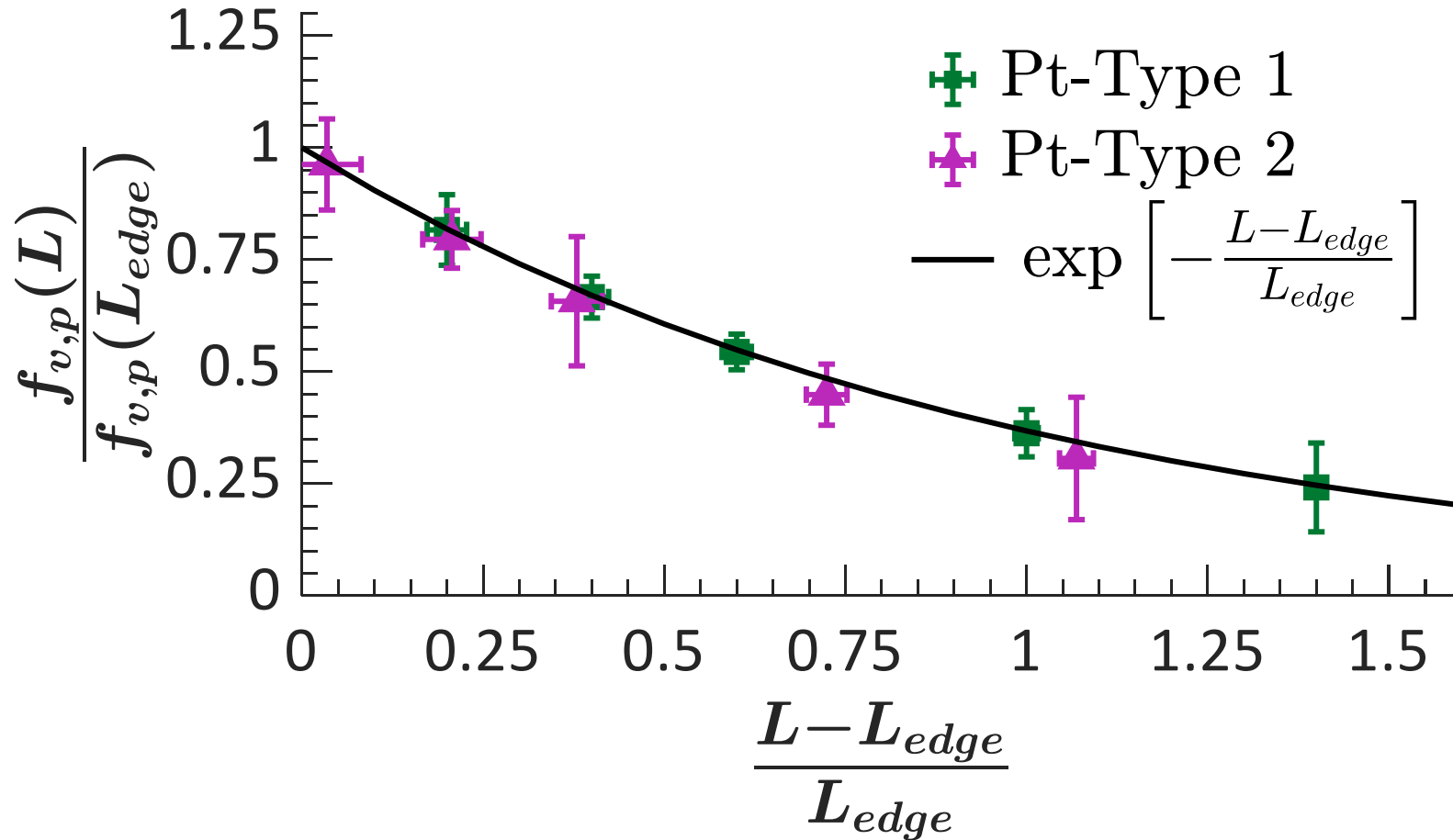
$Q_{vv,p}$:scattering coefficient of the particles



□ Decrease of the scattering coefficient as the nanoparticles are convected downstream of the flame due to dilution in the surrounding gases



- ❑ LII spectral emission decreases at increasing distance from the fuel nozzle, L
- ❑ Nanoparticle vaporization temperature achieved by laser heating (e.g., ~ 5200 K at $L=150$ mm in Pt-type2) increases at increasing L



$$f_{v,p}(L) = \frac{\overline{S_{LII}}(L)}{\overline{S_{LII}}(L_{edge})} f_{v,p}(L_{edge})$$

➤ **Pure Pt assumption:**

$$f_{v,p_{Pt}}(L_{edge}) = 8.70 \cdot 10^{-8}$$

➤ **Pure PtO₂ assumption :**

$$f_{v,p_{PtO_2}}(L_{edge}) = 2.14 \cdot 10^{-7}$$

- We introduce an equation to estimate the volume fraction that predicts the results of LII measurements. The exponential law is typical of (turbulent) diffusion mixing

Particle size

$$\overline{d_{6,3}} = \left(\frac{\overline{d^6}}{\overline{d^3}} \right)^{\frac{1}{3}} = \left(\frac{Q_{vv,p}}{\frac{6}{\pi} \cdot f_{v,p} \cdot \frac{\pi^2}{4\lambda^4} \cdot F(m)} \right)^{\frac{1}{3}}$$

λ : wavelength of the used laser

m : complex refractive index

$F(m)$: scattering function

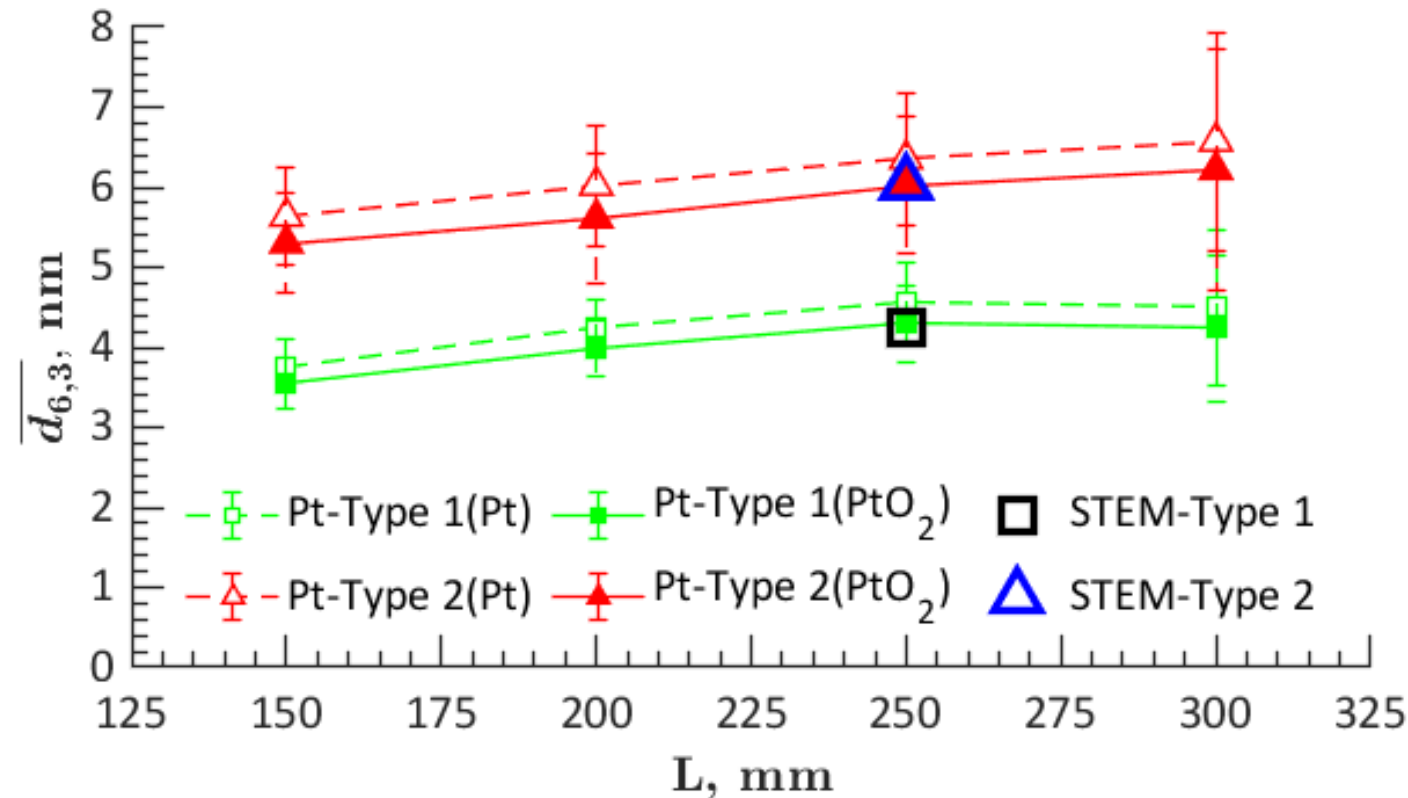
$$F(m) = \left| \frac{m^2 - 1}{m^2 + 2} \right|^2$$

For Pt: $F(m_{Pt}) = 1.23 \pm 0.06$

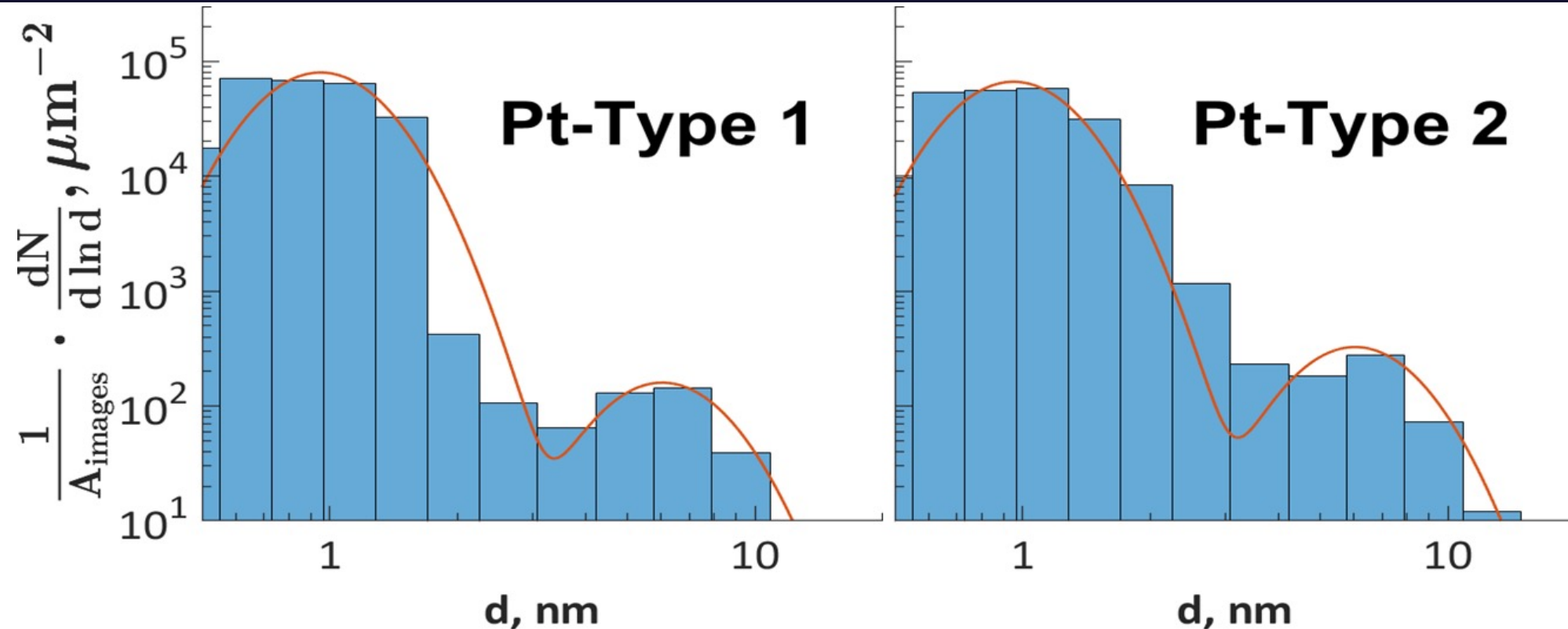
$$f_{v,pPt} (L_{edge}) = 8.70 \cdot 10^{-8}$$

For PtO₂: $F(m_{PtO_2}) = 0.60 \pm 0.03$

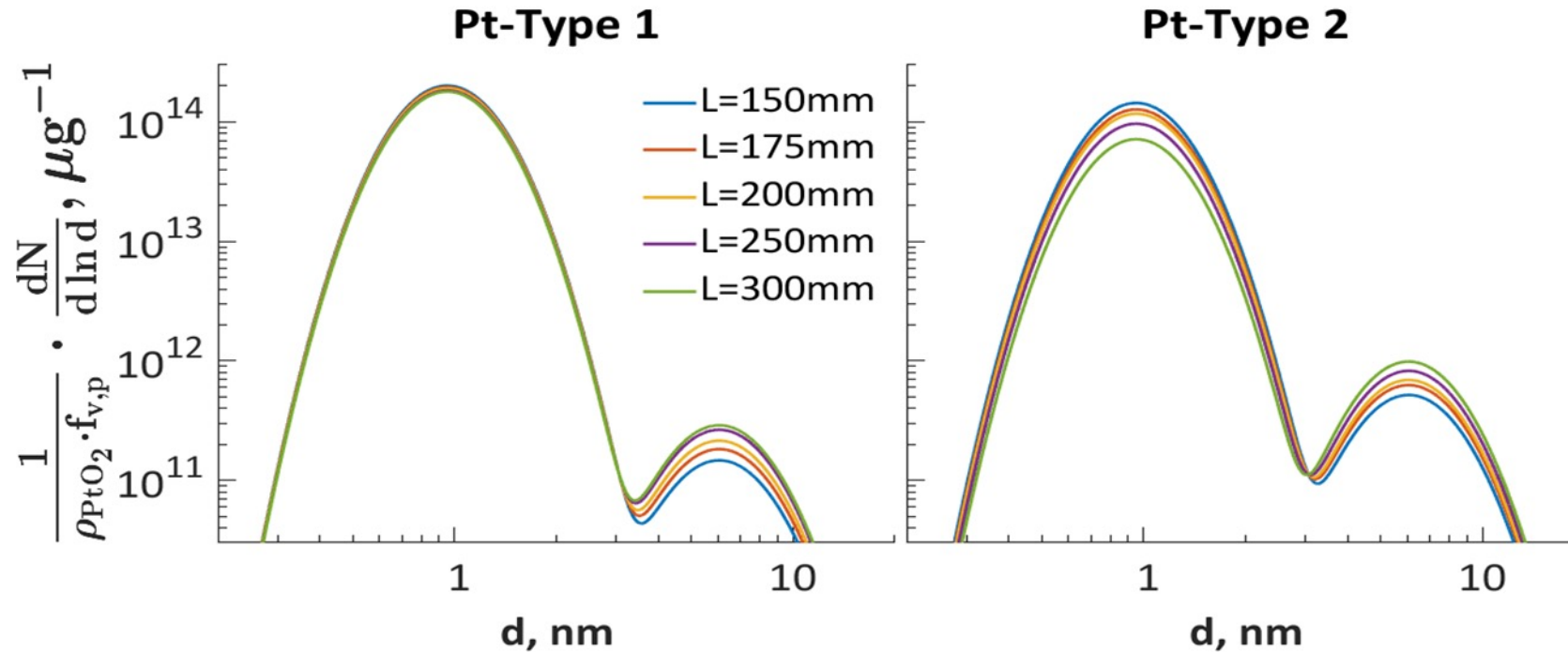
$$f_{v,pPtO_2} (L_{edge}) = 2.14 \cdot 10^{-7}$$



- ❑ The LS equivalent diameter of Pt-Type 2 is larger than the one of Pt-Type 1
- ❑ The results are consistent regardless of the assumption on the oxidation degree of the synthesized particles
- ❑ The LS equivalent diameter is consistent with the HAADF-STEM image analysis in both cases (Pt-Type 1 and Pt-type 2)

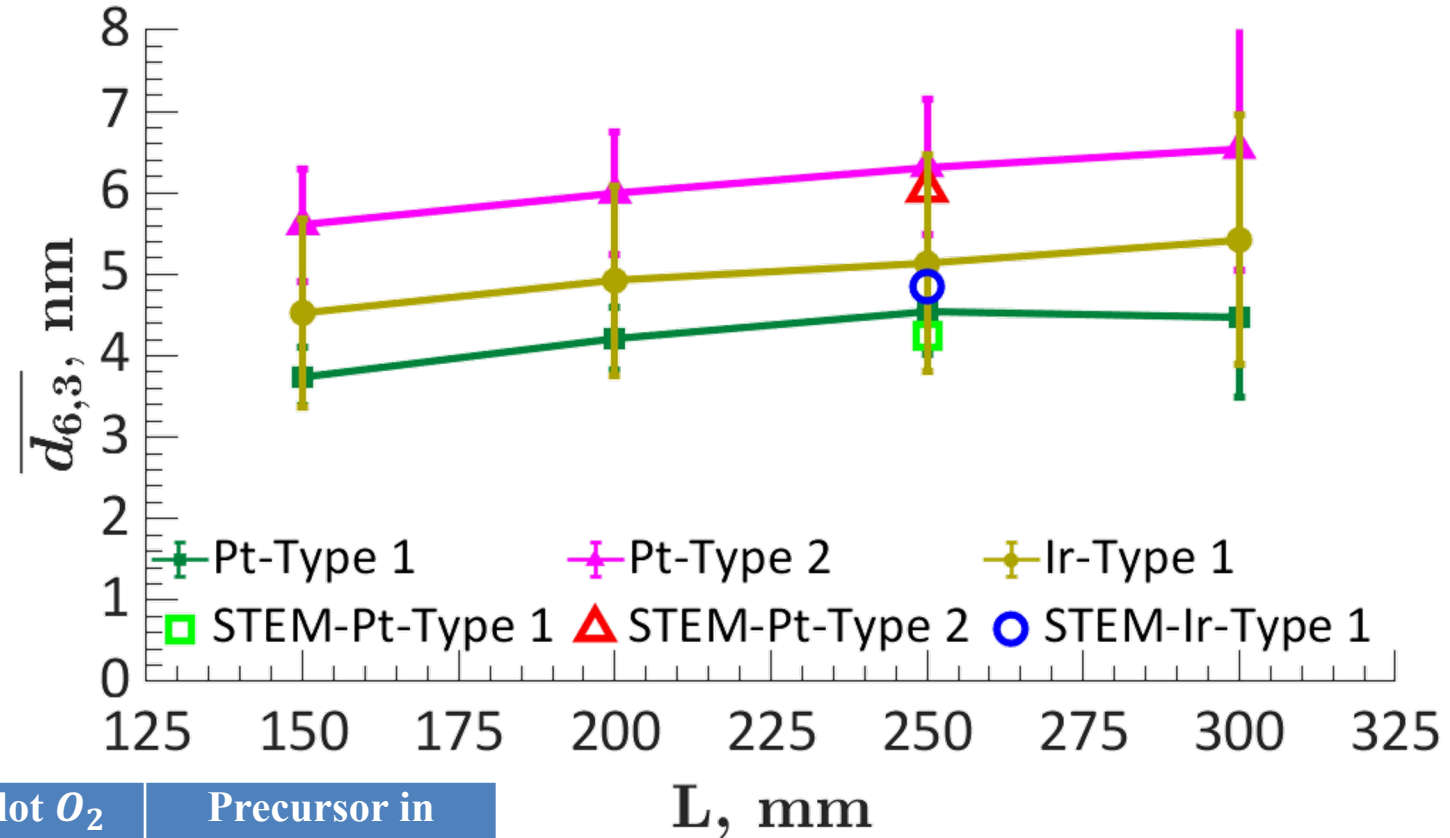


- ❑ Bimodal distribution with first and second mode median diameter positioned at 0.95nm and 6.05nm regardless of the Pt flame type
- ❑ Number concentration of the second mode in the Pt-Type 2 flame is larger than in Pt-Type 1 resulting in larger $d_{6,3}$ measured via LS
- ❑ The sum of the same two log-normal fits microscopy results in both flames

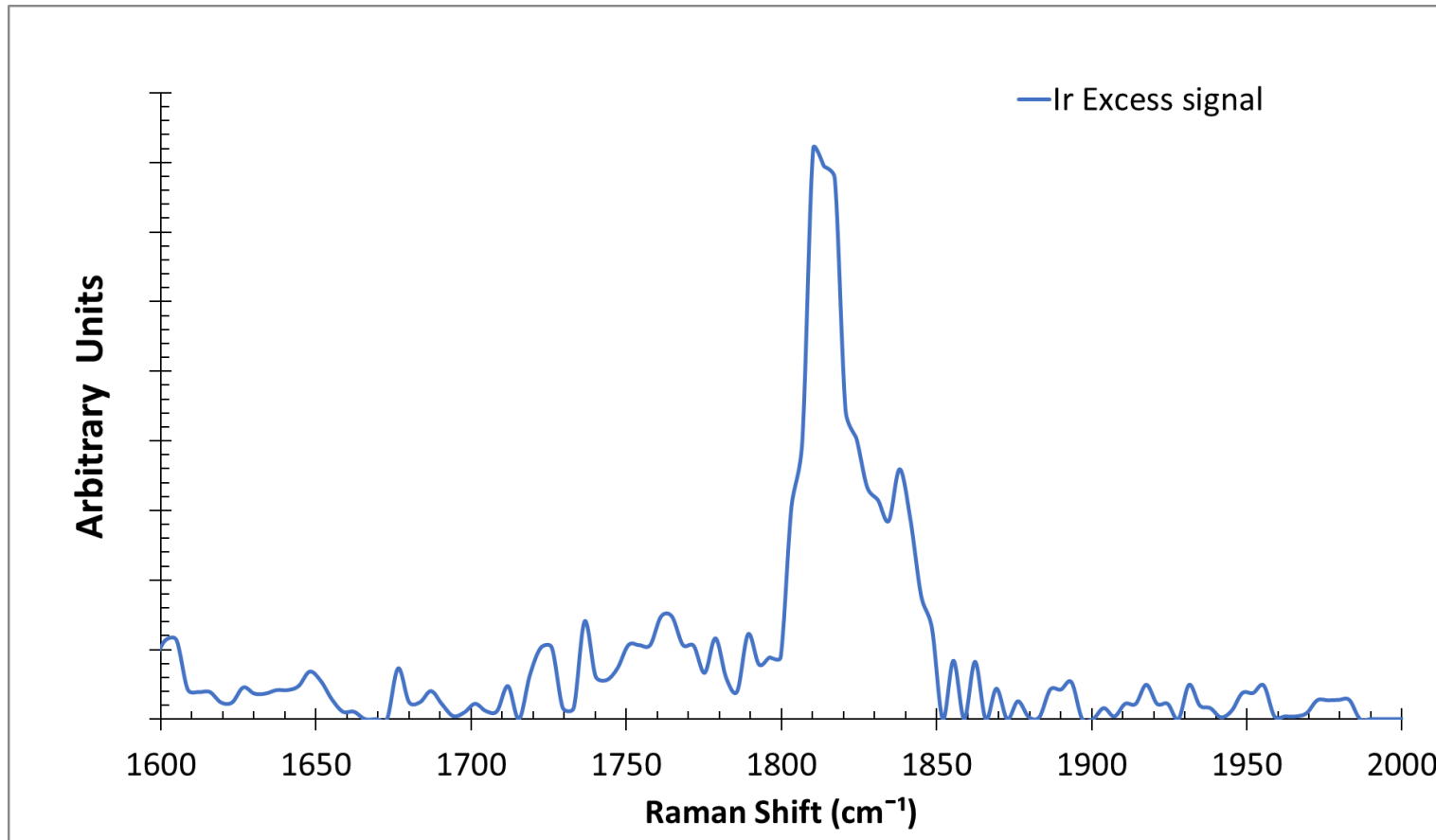


- ❑ Same modes are inferred at all Ls from the $d_{6,3}$ measured by LS
- ❑ The number of particles in the second mode increases as the nanoparticles are convected downstream of the flame resulting in the slight increase of $d_{6,3}$
- ❑ Number concentration of the second mode in the Pt-Type 2 flame is larger than in Pt-Type 1 throughout the flames
- ❑ The synthesized nanoparticles appear to grow at rates that are orders of magnitude slower than the collision rate of non-interacting Brownian nanoparticles

- ❑ The LS equivalent diameter of Ir-Type1 lies between LS equivalent diameter of Pt-Type1 and Pt-Type2
- ❑ The LS equivalent diameter of Ir-Type1 is consistent with the HAADF-STEM image analysis of the samples



Flame name	Liquid fuel mixture (mL/min)	O_2 (SLPM)	Pilot CH_4 flow rate (SLPM)	Pilot O_2 flow rate (SLPM)	Precursor in liquid fuel
Pt-Type 1	4	7.3	0.55	0.55	10 mM PtAcAc
Pt-Blank 1	4	7.3	0.55	0.55	-
Pt-Type 2	7	11	0.75	0.75	10mM PtAcAc
Pt-Blank 2	7	11	0.75	0.75	-
Ir-Type 1	8	12	0.75	0.75	9mM IrAcAc
Ir-Blank 1	8	12	0.75	0.75	-



- ❑ A Raman peak is detected in the Ir flame at $\sim 1820 \text{ cm}^{-1}$ which is not present in the blank flame.
- ❑ Preliminary investigation suggests that the peak is, due to the presence of carbonyl groups on the surface of the synthesized nanoparticles

- ❑ Identified a simple methodology for rapidly predicting the axial profile of the nanoparticle volume fraction downstream of two RSDT flames
- ❑ Pt nanoparticles withstand progressively higher vaporization temperatures as they are aging in the flame, possibly due to changes in their phase and/or degree of oxidation
- ❑ The PSDs are composed of two lognormal modes centered at approximately 1 nm and 6 nm, with the relative number of nanoparticles belonging to the larger mode being determined by the RSDT flame operating parameters for the investigated precursor solution
- ❑ The synthesized nanoparticles appear to grow at rates that are orders of magnitude slower than the collision rate of non-interacting Brownian nanoparticles
- ❑ Preliminary Raman results of Ir flame suggest the attachment of carbonyl groups on the surface of the synthesized nanoparticles

The authors would like to thank:

- Funding Agency
 - Department of Energy (DE-EE0008427)
- Center for Clean Energy Engineering of the University of Connecticut

Flame, Aerosol, and Nano
Technologies Laboratory
(FANTastic Lab)



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Energy Engineering

Questions



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